



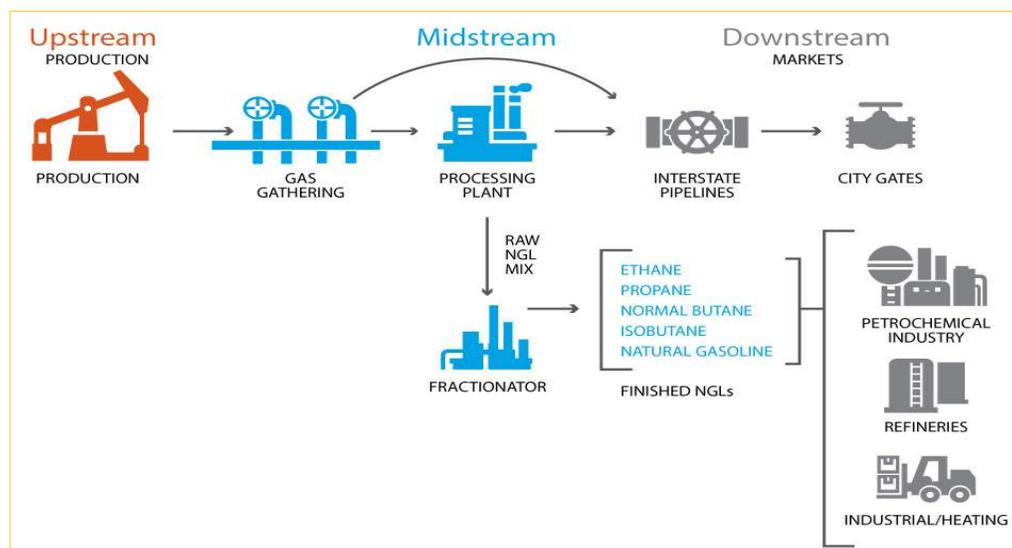
## Problem-Based Learning on Incorporation of Data Analysis Skills into a Senior Course

**Helen H. Lou, Yifan Chen, Ravinder Singh**

Dan F. Smith Department of Chemical & Biomolecular Engineering  
Lamar University

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AIChE Annual Meeting, Boston, MA

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**Data** → **Sustainability**

**ChE + Data Skills**

**ECONOMIC**

- Economic growth and resilience
- Affordability
- Energy security
- Process efficiency
- Outputs of desired products

**ENVIRONMENTAL**

- Water quality and quantity
- Soil quality
- Air quality
- Greenhouse gas emissions
- Biodiversity and wildlife

**SOCIAL**

- Jobs and workforce development
- Health and well-being
- Food security
- Social acceptability

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**ChE + Data Skills**

**Traditional ChE Skills**

- Chemistry
- Thermodynamics
- Reaction kinetics
- Unit operations
- Process design
- Process control
- First-principles based process modeling

**Data Skills**

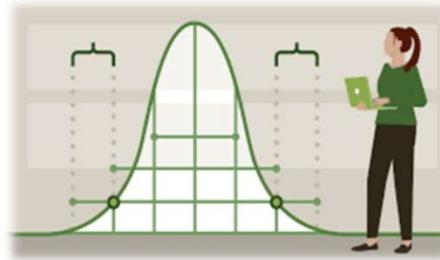
- Statistics
- Data preprocessing
- Feature engineering
- Representative ML algorithms
- Evaluation matrix
- Uncertainty
- Time series analysis
- Data analytics using spreadsheet/python/R
- Basics of database management
- Data scraping and data crawling

<https://www.linkedin.com/pulse/cheche-data-skills-compassion-helen-lou/?trackingId=009Zob42K62M8tfa0osuNA%3D%3D>

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## Data Skills

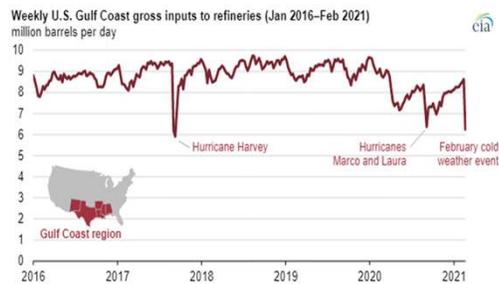
Spreadsheet is popular in the plants, and it is highly desirable for chemical engineering students to learn how to analyze data using an Excel spreadsheet



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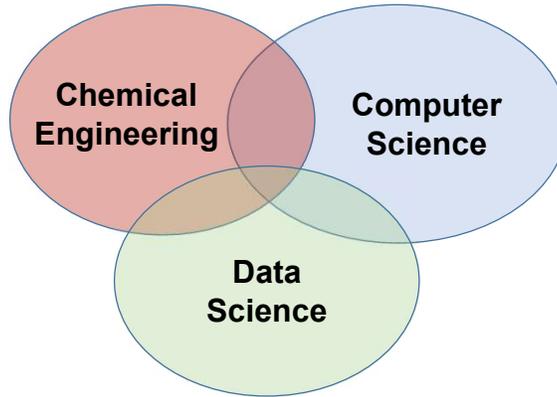
## Data Skills

Chemical engineers should understand and be able to handle uncertainties in production



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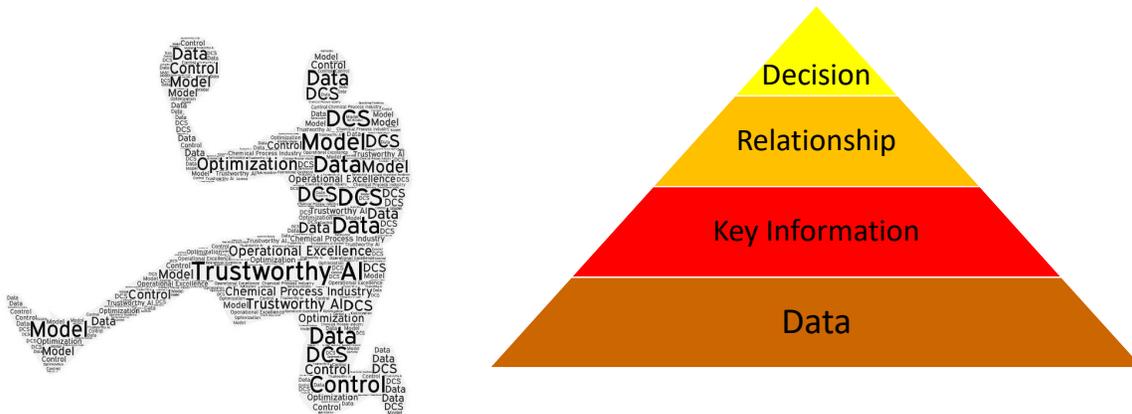
## Combined Expertise for Success



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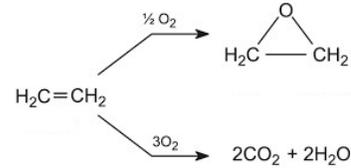
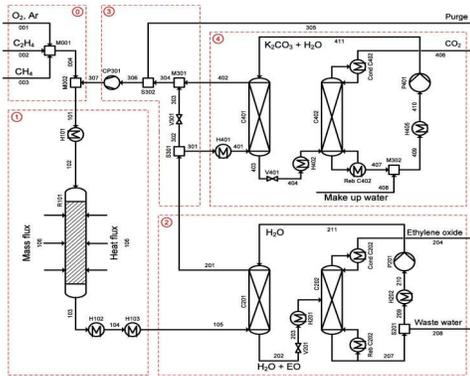
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## Using AI for Process Operational Excellence



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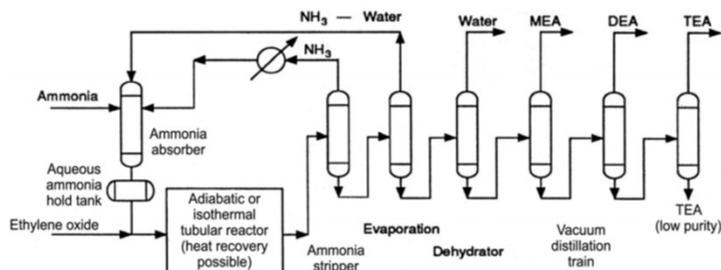
## Example 1: An Ethylene Oxide Process



- Selectivity improvement: >3%
- Annual Profit increase (\$/yr): ~4.3 Million

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## Example II: An Ethanolamines Process



MEA: Monoethanolamine  
 DEA: Diethanolamine  
 TEA: Triethanolamine

- Reduce undesirable byproducts by 66%
- Save \$0.3/lb

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## Example III: Combustion Modeling and Predictive Flare Control

### Background: EPA Refinery Sector Rule (RSR)

- Destruction efficiency (DRE)  $\geq 98\%$  or
- Combustion efficiency (CE  $\geq 96.5\%$ )
- No visible smoke
- Pilot flame present all the time
- Combustion zone net heating value (NHVcz)  $\geq 270$  BTU/ft<sup>3</sup> on a 15-minute rolling average



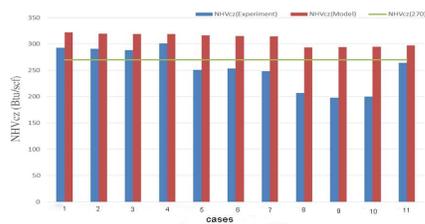
### Objective: Optimize the Flare Operating Parameters (steam/air injection rate and supplement fuel gas flowrate)

- Meet compliance of Combustion Efficiency (CE)/Destruction Efficiency (DRE) and opacity (no visible smoke)
- Minimize operating cost

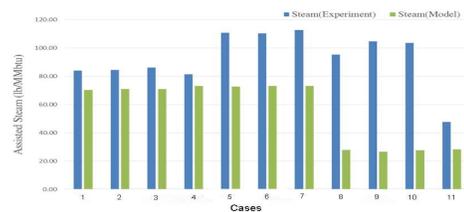
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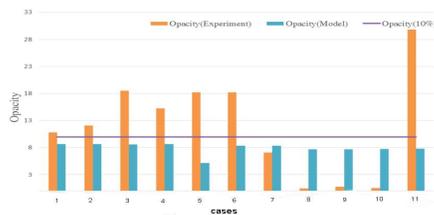
### Optimized NHVcz vs. Historical Data



### Optimized Assisted Steam vs. Historical Data



### Optimized Opacity vs. Historical Data



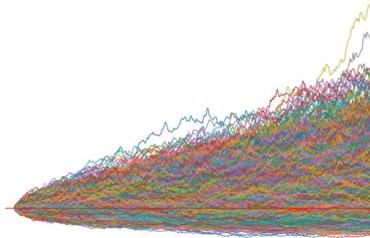
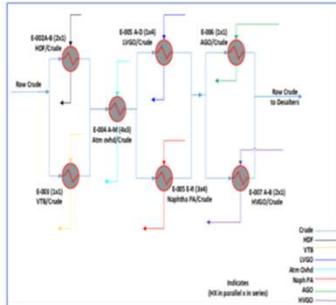
**Net cost saving:**  
**Avg – 38.5%**  
**Min – 16.0%**  
**Max – 74.6%**

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## PBL: Refinery CDU Heat Exchangers Fouling Diagnosis



Monte Carlo Simulation



Lou, H. H., Y. Chen, and R. Singh, "Problem-Based Learning on Incorporation of Data Analysis Skills into Chemical Engineering Senior Advanced Analysis Course," *Smart and Sustainable Manufacturing Systems* (March 2021), DOI: 10.1520/SSMS20200027.

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## Closing the Skills Gap in the "Advanced Analysis" Course

- Recap of basic statistics: this include how to describe the characteristics of a given data set using terms of mean, median, mode, standard error, standard deviation, sample variance, kurtosis and skewness, confidence level, etc.
- Identifying the outliers
- Correlation
- Regression
- Deal with uncertainty
- Time series analysis
- Optimization

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## Problem Based Learning (PBL) Approach

- A student-centered approach
- Team work to solve open-ended problem
- Problem drives the motivation and learning



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## Skills Developed in PBL

- Team work
- Managing projects and holding leadership roles
- Oral and written communication
- Self-awareness and evaluation of group processes
- Working independently
- Critical thinking and analysis



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## Monte Carlo Methods Applications in Chemical Engineering

- A statistical approach to provide approximate solutions to mathematically complex optimization or simulation problems faced with uncertainty by using random sequences of numbers.
- Monte Carlo simulations are used to model the probability of different outcomes in a process that cannot easily be predicted because of the intervention of random variables.
- In an application of asset reliability, heat exchanger performance was modeled considering manufacturing tolerances and uncertain flow distribution.

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## Case Study

- Students introduced to
  - fundamentals of statistics
  - outlier detection using IQR
  - Monte Carlo simulation
- The students were divided into groups of 4–5 people each
- They were asked to figure out which heat exchangers in a refinery need to be cleaned with the help of Monte Carlo simulation and statistics analysis.

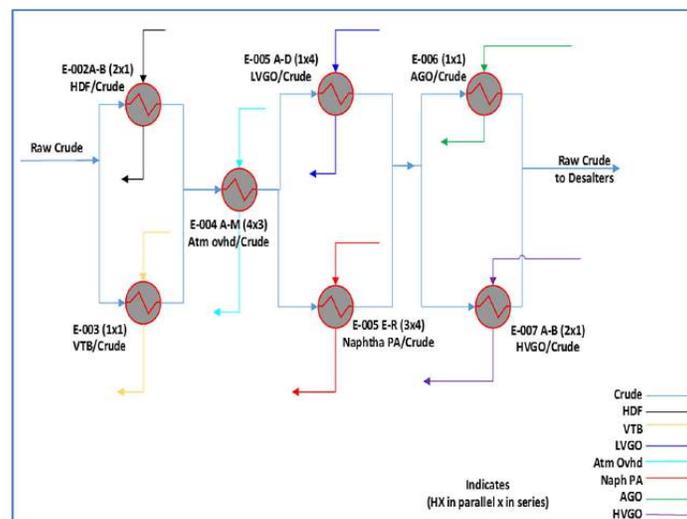
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## Case Study

- Two years of related operation data from a crude distillation unit in a refinery
- The heat exchanger bank consists of seven counter current heat exchangers
- Raw crude on the tube side

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## Schematic Flow of the Process



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## Process Data

- Flow rates, bph
- Crude densities, lb/ft<sup>3</sup>
- Outlet and Inlet temperatures, F
- Exchanger area, ft<sup>2</sup>
- Number of shells
- Heat capacity of the fluid, C<sub>p</sub>
- Designed value of heat exchange rate, Q<sub>Design</sub>
- Heat transfer coefficient during normal service, U<sub>Service</sub>

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## Fundamental Equations

$$(1) \text{LMTD} = \frac{[(T_{i1} - T_{o2}) - (T_{o1} - T_{i2})]}{\ln[(T_{i1} - T_{o2}) - (T_{o1} - T_{i2})]}$$

Where:

T<sub>i1</sub> = shell side inlet temperature,

T<sub>i2</sub> = shell side outlet temperature,

T<sub>o1</sub> = tube side inlet temperature, and

T<sub>o2</sub> = tube side outlet temperature.

$$(2) U_{\text{values}} = \frac{Q_{\text{Design}}}{A \cdot \text{LMTD}}$$

Where:

Q<sub>Design</sub> = design value of heat exchange rate, and

A = heat exchange area.

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## Sample of LMTD & HT Coeff Values

**TABLE 1**  
Sample of LMTD and heat transfer coefficients values of E4

| Design    | LMTD | U (Actual) |
|-----------|------|------------|
| 5/1/2019  | 59   | 249        |
| 4/30/2019 | 59   | 249        |
| 4/29/2019 | 59   | 251        |
| 4/28/2019 | 58   | 255        |
| 4/27/2019 | 58   | 255        |
| 4/26/2019 | 56   | 261        |
| 4/25/2019 | 60   | 246        |
| 4/24/2019 | 61   | 243        |
| 4/23/2019 | 61   | 243        |
| 4/22/2019 | 58   | 255        |
| 4/21/2019 | 55   | 266        |
| 4/20/2019 | 53   | 279        |
| 4/19/2019 | 55   | 270        |
| 4/18/2019 | 58   | 254        |
| 4/17/2019 | 61   | 243        |
| 4/16/2019 | 59   | 249        |
| 4/15/2019 | 57   | 259        |
| 4/14/2019 | 57   | 257        |
| 4/13/2019 | 63   | 233        |
| 4/12/2019 | 60   | 244        |
| 4/11/2019 | 64   | 231        |
| 4/10/2019 | 63   | 235        |
| 4/9/2019  | 60   | 246        |
| 4/8/2019  | 61   | 240        |
| 4/7/2019  | 64   | 231        |
| 4/6/2019  | 63   | 234        |
| 4/5/2019  | 64   | 231        |
| 4/4/2019  | 63   | 234        |

Note: Highlighting indicates that the heat exchanger is functioning at or very near its  $U_{design}$  value

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## Sample of Process Data

**TABLE 2**  
Sample of process data and some statistics data for a heat exchanger

| Design              | Raw Crude (Tube Side) |                             | VTB (Shell Side) |                             | Raw Crude (Tube Side) |              | VTB (Shell Side) |              | Area, ft <sup>2</sup> |       | U    |
|---------------------|-----------------------|-----------------------------|------------------|-----------------------------|-----------------------|--------------|------------------|--------------|-----------------------|-------|------|
|                     | Flow Rate, bph        | Density, lb/ft <sup>3</sup> | Flow Rate, bph   | Density, lb/ft <sup>3</sup> | Temp In, °F           | Temp Out, °F | Temp In, °F      | Temp Out, °F | LMTD                  | 3,561 |      |
| 11/21/2016          | 1,159.15              | 57.63                       | 2,650.08         | 65.00                       | 80                    | 106          | 420              | 438          | 335                   | ...   | 16.5 |
| 11/20/2016          | 1,195.13              | 57.66                       | 2,464.41         | 65.00                       | 82                    | 108          | 440              | 459          | 354                   | ...   | 15.6 |
| 11/19/2016          | 1,202.67              | 57.60                       | 2,324.27         | 65.00                       | 87                    | 111          | 442              | 460          | 352                   | ...   | 15.7 |
| 11/18/2016          | 1,207.68              | 57.69                       | 2,323.83         | 65.00                       | 90                    | 114          | 444              | 462          | 351                   | ...   | 15.7 |
| 11/17/2016          | 1,207.02              | 57.73                       | 2,399.81         | 65.00                       | 87                    | 111          | 439              | 457          | 348                   | ...   | 15.9 |
| 11/16/2016          | 1,165.46              | 57.52                       | 2,332.02         | 65.00                       | 87                    | 111          | 439              | 458          | 349                   | ...   | 15.8 |
| 11/15/2016          | 1,138.58              | 57.52                       | 2,250.32         | 65.00                       | 86                    | 106          | 389              | 395          | 295                   | ...   | 18.7 |
| 11/14/2016          | 1,170.74              | 57.52                       | 1,989.48         | 65.00                       | 85                    | 105          | 371              | 373          | 277                   | ...   | 19.9 |
| 11/13/2016          | 1,193.45              | 57.49                       | 2,011.20         | 65.00                       | 86                    | 105          | 370              | 372          | 275                   | ...   | 20.1 |
| 11/12/2016          | 1,146.68              | 57.52                       | 1,979.28         | 65.00                       | 85                    | 102          | 369              | 370          | 276                   | ...   | 20.0 |
| 11/11/2016          | 1,207.38              | 57.51                       | 1,924.73         | 65.00                       | 87                    | 105          | 370              | 370          | 274                   | ...   | 20.1 |
| 11/10/2016          | 1,254.88              | 57.71                       | 2,002.22         | 65.00                       | 88                    | 111          | 369              | 366          | 268                   | ...   | 20.6 |
| 11/9/2016           | 1,180.57              | 57.71                       | 2,055.04         | 65.00                       | 93                    | 117          | 365              | 362          | 258                   | ...   | 21.4 |
| 11/8/2016           | 1,080.05              | 57.71                       | 1,675.12         | 65.00                       | 95                    | 130          | 358              | 345          | 238                   | ...   | 23.2 |
| 11/7/2016           | 1,012.97              | 57.71                       | 3,512.52         | 65.00                       | 94                    | 141          | 350              | 326          | 220                   | ...   | 25.0 |
| 11/6/2016           | 885.88                | 57.71                       | ...              | 65.00                       | 88                    | 114          | 274              | 256          | 164                   | ...   | 33.6 |
| Q1                  | 2,285.31              | 56.45                       | 2,030.81         | 65                          | 80.73                 | 100.36       | 384.43           | 382.95       | 288.33                | ...   | ...  |
| Q3                  | 3,552.83              | 57.41                       | 2,370.57         | 65                          | 93.82                 | 109.06       | 396.45           | 399.01       | 302.74                | ...   | ...  |
| IQR                 | 1,267.52              | 0.95                        | 339.76           | 0.001                       | 13.08                 | 8.70         | 12.01            | 16.06        | 14.41                 | ...   | ...  |
| Upper bound         | 5,454.11              | 58.85                       | 2,880.23         | 65                          | 113.46                | 122.11       | 414.48           | 423.11       | 324.37                | ...   | ...  |
| Lower bound         | 384.03                | 55.01                       | 1,521.16         | 65                          | 61                    | 87.31        | 366.41           | 358.85       | 266.71                | ...   | ...  |
| Avg. (w/o outliers) | 2,658.85              | 56.85                       | 2,202.42         | 65                          | 86.66                 | 104.89       | 390.61           | 391.22       | 295.83                | ...   | ...  |
| STD                 | 868.25                | 0.55                        | 256.31           | 0.01                        | 7.88                  | 6.91         | 8.60             | 12.32        | 10.17                 | ...   | ...  |

Note: Avg. = average; STD = Standard Deviation; VTB = vacuum tower bottoms; w/o = without. Highlighting indicates that the heat exchanger is functioning at or very near its  $U_{design}$  value.

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## Monte Carlo Simulation

**TABLE 3**  
Monte Carlo simulation on E4

| Monte Carlo RAND | LMTD  | U (Calculated) |
|------------------|-------|----------------|
| 1                | 76.39 | 19.30          |
| 2                | 64.93 | 22.71          |
| 3                | 80.49 | 18.32          |
| 4                | 67.37 | 21.89          |
| 5                | 73.39 | 20.09          |
| 6                | 73.38 | 20.09          |
| 7                | 66.10 | 22.31          |
| 8                | 71.00 | 20.77          |
| 9                | 65.95 | 22.36          |
| 10               | 69.72 | 21.15          |
| 11               | 70.36 | 20.96          |
| 12               | 69.42 | 21.24          |
| 13               | 69.86 | 21.11          |
| 14               | 63.57 | 23.20          |
| 15               | 73.61 | 20.03          |
| 16               | 69.61 | 21.18          |
| 17               | 75.94 | 19.42          |
| 18               | 68.74 | 21.45          |
| 19               | 81.91 | 18.00          |
| 20               | 70.55 | 20.90          |
| 21               | 69.13 | 21.33          |
| 22               | 74.59 | 19.77          |
| 23               | 75.82 | 19.19          |

Note: RAND is a mathematical function in Microsoft Excel used to generate random numbers.

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## Statistical Results of MC Simulation

Descriptive statistics of Monte Carlo simulation on E4

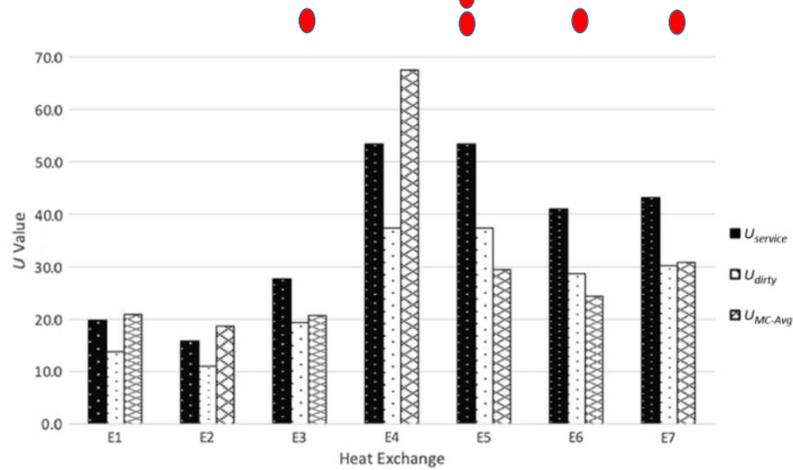
### Descriptive Statistics

|                          |           |
|--------------------------|-----------|
| Mean                     | 20.73     |
| Standard error           | 0.01      |
| Median                   | 20.64     |
| Mode                     | #N/A      |
| Standard deviation       | 1.42      |
| Sample variance          | 2.01      |
| Kurtosis                 | 0.33      |
| Skewness                 | 0.44      |
| Range                    | 11.26     |
| Minimum                  | 16.09     |
| Maximum                  | 27.35     |
| Sum                      | 207,276.4 |
| Count                    | 10,000    |
| Confidence level (95.0%) | 0.03      |

Note: #N/A = Not Applicable.

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## Cleaning Recommendations



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## Cleaning Recommendations

**TABLE 5**

Cleaning recommendations/ranking for the heat exchangers

| Exchangers | $U_{service}$ | $U_{dirty}$ | $U_{MC-Avg}$ | Clean? | Rank |
|------------|---------------|-------------|--------------|--------|------|
| E1         | 19.8          | 13.9        | 21.0         | No     | 5    |
| E2         | 15.8          | 11.1        | 18.7         | No     | 6    |
| E3         | 27.7          | 19.4        | 20.7         | Yes    | 3    |
| E4         | 53.4          | 37.4        | 67.5         | No     | 7    |
| E5         | 53.4          | 37.4        | 29.5         | Yes    | 1    |
| E6         | 41.0          | 28.7        | 24.3         | Yes    | 2    |
| E7         | 43.2          | 30.2        | 30.9         | Yes    | 4    |

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## Discussion

- The calculated U values for each heat exchanger were compared with the design U value for each of the heat exchangers. If the calculated U value was 70 % less than the design U value, cleaning was recommended.
- It is possible that the U value might never meet the design U value, even after a full-service cleaning. This gives the engineer a better idea of what type of recommendation to make in terms of cleaning/servicing.
- Based on the data analysis of these heat exchangers, the students recommended which heat exchangers should be cleaned. The type of cleaning (shell only or both shell and bundle) can be determined through looking at the past maintenance history.

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## Conclusion

- This project was well received by the students
- Some students eventually worked in the refineries as process engineers or maintenance engineers after graduation. This project helped them obtain some essential skills needed
- It is demonstrated that a PBL approach is highly effective for teaching data analytics.

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## Thoughts

- Understand our customers - students
- Communicate with the industry
- Be adaptive
- Share the experience

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## Acknowledgement

- Industrial partner
- Lamar University Center for Midstream Management and Science

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*Thank  
you*

A close-up image of a fountain pen nib, showing the gold-colored metal and the blue ink reservoir.

**Helen Lou, Ph.D., Professor, AIChE Fellow**  
**Dan F. Smith Department of Chemical & Biomolecular Engineering**  
**Associate Director-Research, Center for Midstream Management and Science**  
**Lamar University**  
**Email: [helen.lou@lamar.edu](mailto:helen.lou@lamar.edu)**  
**Phone: 409-880-8207**