

**Final Exam**  
**ChE 231**  
**Spring 2019**

Problem 1 (45 pts). Consider a continuous stirred tank used to dissolve a gas component into a liquid. Mass balances on the gas and liquid phases yield the following linear ODE system,

$$\begin{aligned}\frac{dC_g}{dt} &= \frac{q_g}{V_g}(C_{g,f} - C_g) - k_L a(C^* - C_L) \\ \frac{dC_L}{dt} &= -\frac{q_L}{V_L}C_L + k_L a(C^* - C_L)\end{aligned}$$

where  $C_g$  and  $C_L$  are molar concentrations of the component in the gas and liquid phases,  $q_g$  and  $q_L$  are volumetric flow rates of the gas and liquid phases,  $V_g$  and  $V_L$  are the volumes of the gas and liquid phases,  $C_{g,f}$  is the molar concentration of the gas component fed to the tank, and  $k_L a$  is the gas-liquid mass transfer coefficient. The saturated liquid concentration of the component is calculated as  $C^* = HC_g$ , where  $H$  is the Henry's law constant.

1. (5 points) Given the parameter values  $\frac{q_g}{V_g} = 2$ ,  $\frac{q_L}{V_L} = 1$ ,  $k_L a = 1$ ,  $H = 0.5$  and  $C_{g,f} = 4.5$  show that the ODE system can be written as,

$$\frac{d}{dt} \begin{bmatrix} C_g \\ C_L \end{bmatrix} = \begin{bmatrix} -2.5 & 1 \\ 0.5 & -2 \end{bmatrix} \begin{bmatrix} C_g \\ C_L \end{bmatrix} + \begin{bmatrix} 9 \\ 0 \end{bmatrix} = \mathbf{A} \begin{bmatrix} C_g \\ C_L \end{bmatrix} + \mathbf{b}$$

2. (10 points) Show that the ODE system has the steady-state solution  $\bar{C}_g = 4$  and  $\bar{C}_L = 1$  and express the ODE system in the form  $\frac{d\mathbf{y}'}{dt} = \mathbf{A}\mathbf{y}'$
3. (15 points) Show that the eigenvalues and eigenvectors of the  $\mathbf{A}$  matrix are,

$$\lambda_1 = -1.5, \quad \mathbf{x}^{(1)} = \begin{bmatrix} 1 \\ 1 \end{bmatrix}, \quad \lambda_2 = -3, \quad \mathbf{x}^{(2)} = \begin{bmatrix} 2 \\ -1 \end{bmatrix}$$

4. (15 points) Given the initial conditions  $C_g(0) = 4.5$  and  $C_L(0) = 0$ , find the solutions  $C_g(t)$  and  $C_L(t)$ . Sketch the solutions.

Problem 2 (35 pts). Consider a continuous stirred tank bioreactor used to produce an microbial enzyme. Mass balances on the cellular biomass and secreted enzyme yield the following nonlinear ODE system,

$$\begin{aligned}\frac{dX}{dt} &= -DX + \mu(P)X = f_1(X, P) \\ \frac{dP}{dt} &= -DP - k_d P + vX = f_2(X, P)\end{aligned}$$

where  $X$  is the biomass concentration,  $P$  is the enzyme concentration,  $D$  is the dilution rate,  $k_d$  is the enzyme degradation rate, and  $v$  is the enzyme synthesis rate. The cellular growth rate  $\mu$  is inhibited by enzyme  $\mu(P) = \mu_m (1 - P/P_m)$  where  $\mu_m$  is the maximum growth rate and  $P_m$  is the maximum enzyme concentration.

- (10 points) Given the parameter values  $D = 0.1$ ,  $\mu_m = 0.2$ ,  $v = 0.06$ ,  $k_d = 0.02$  and  $P_m = 10$ , show that the ODE system has the steady state  $\bar{X} = 10$  and  $\bar{P} = 5$ .
- (15 points) Show that linearization of the ODE system at the steady state yields the linear ODE system,

$$\frac{d}{dt} \begin{bmatrix} X' \\ P' \end{bmatrix} = \begin{bmatrix} 0 & -0.2 \\ 0.06 & -0.12 \end{bmatrix} \begin{bmatrix} X' \\ P' \end{bmatrix} = \mathbf{A} \begin{bmatrix} X' \\ P' \end{bmatrix}$$

- (10 points) Calculate the eigenvalues of the  $\mathbf{A}$  matrix and determine if the dynamic response is stable/unstable and oscillatory/non-oscillatory.

Problem 3 (20 pts) The bioreactor considered in Problem 2 was used to generate the following data for the effect of the dilution rate  $D$  on the steady-state biomass concentration  $X$ ,

Experiment	1	2	3	4	5	6
$D$	0.04	0.05	0.06	0.07	0.08	0.09
$X$	8.00	8.75	9.33	9.75	10.00	10.08

- (10 points) Perform linear regression analysis based on statistics to find the slope and intercept of the linear model  $X = k_1 D + k_0$ .
- (10 points) Perform linear regression analysis based on the least-squares method to show that the two methods yield the same linear model.