



WPI

**2015 ASEE ANNUAL
CONFERENCE & EXPOSITION**

*Making Value
for Society*

A Unit Operations Laboratory Experiment Combined with Computer Simulation to Teach PID Controller Tuning

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WPI

Curriculum

3 Projects
12 of 14 Core Courses

Term → Year ↓	A	B	C	D
First Year		Intro to ChE		
Sophomore <u>HUA Project</u>	Chemical Engineering Fundamentals	Elementary Chemical Processes	Applied Thermodynamics	Advanced Chemical Processes
Junior <u>Interdisciplinary Project</u>	Fluid Mechanics	Heat Transfer	Mass Transfer	Kinetics and Reactor Design
Senior <u>Research Project</u>	Unit Operations Laboratory I	Unit Operations Laboratory II	Process Control	Applied Math
	Process Design and Economics	<u>Capstone Design</u>	Worcester Polytechnic Institute	

Motivation

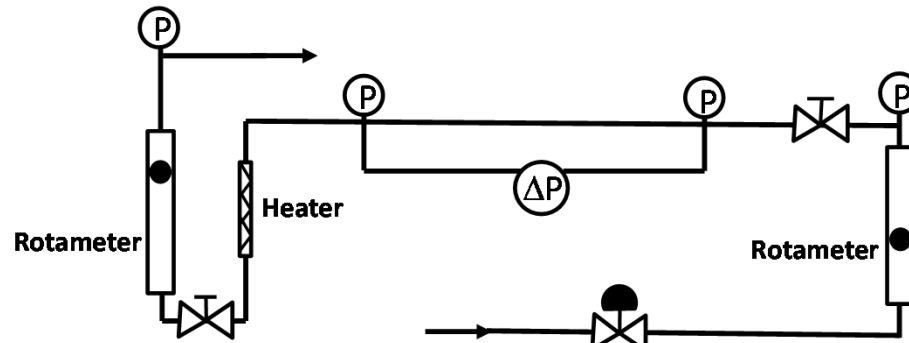
- Only 50 % of student took process control class
- We and ABET wanted more exposure to control in the curriculum

Tim Wescott, "PID Without a PhD", Embedded Systems Programming, October, 2000, 86-108.

"PID (proportional, integral, derivative) control is not as complicated as it sounds. Follow these simple implementation steps for quick results."

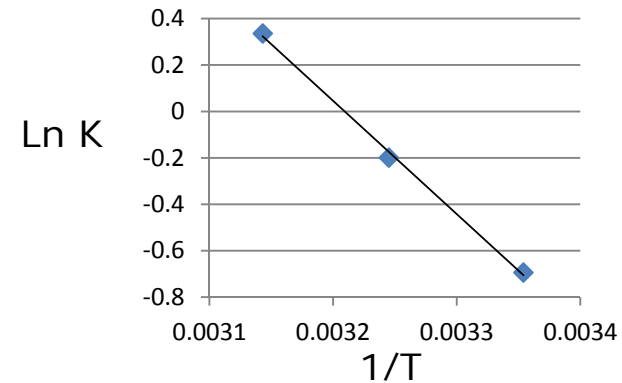
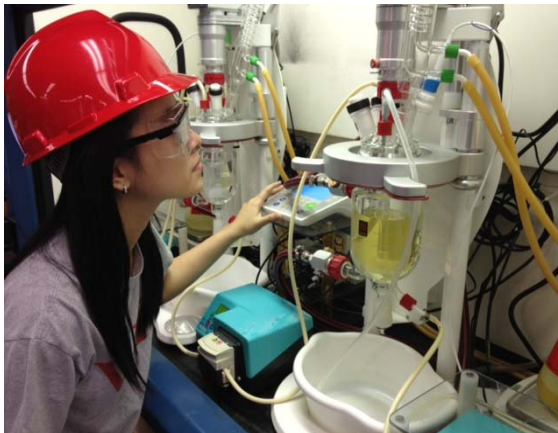
Process Control in UO Lab?

- Computer control of a heat exchanger no longer works
- T control for oven on packed bed reactor experiment
- Control of in-line heater in air flow experiment



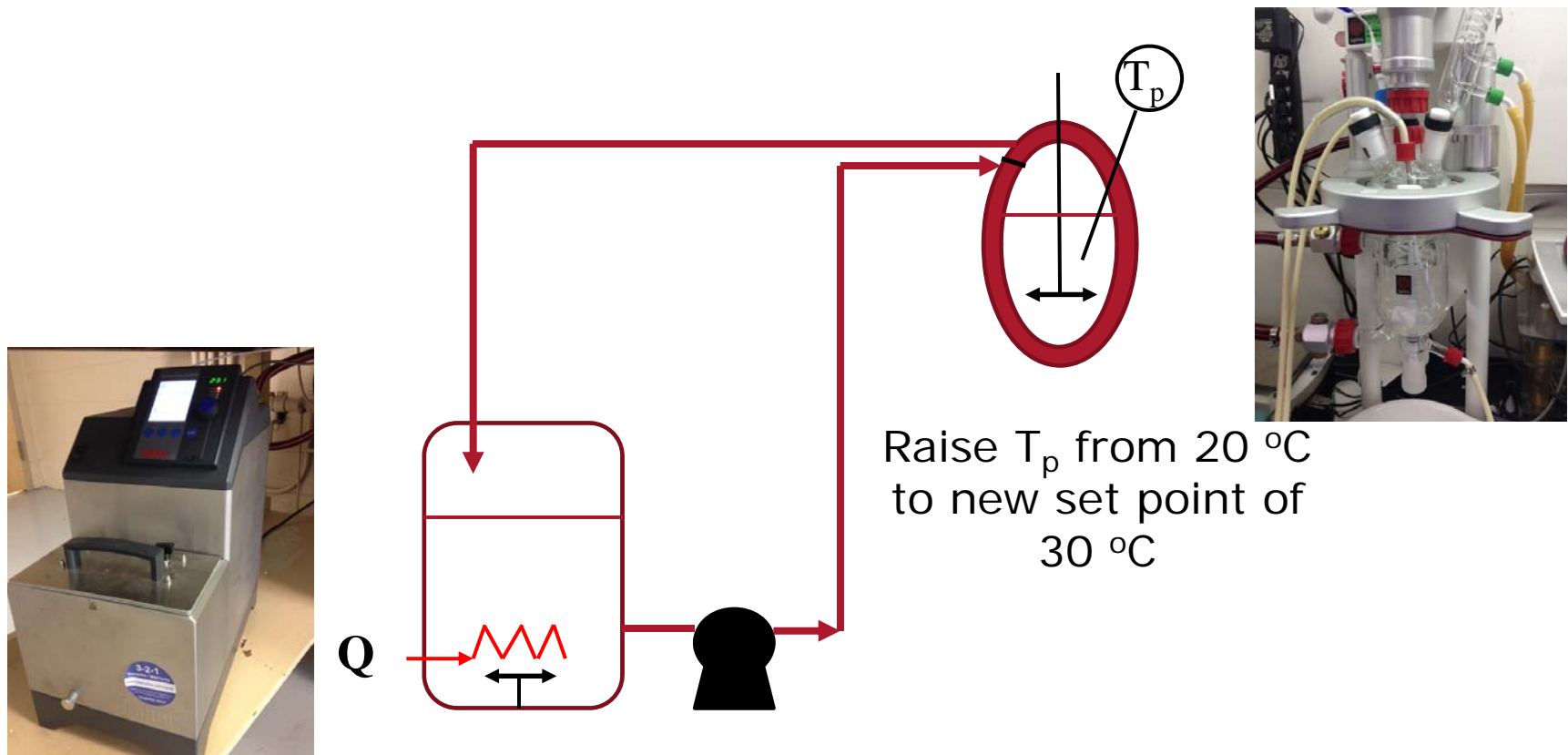
Omega controller difficult to program

- Temperature control of biodiesel experiment batch reactor



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Temperature Control of Batch Reactor



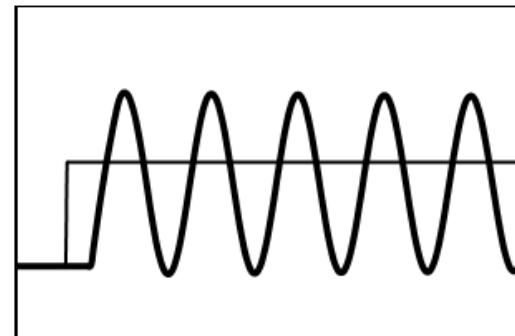
$$Q(t) = Q_o \left[K_p E(t) + K_i \int_0^t E(t) dt + K_d \frac{dE(t)}{dt} \right]$$
$$E(t) = T_{sp} - T_p$$

Temperature Control of Batch Reactor

Limitations

- 30 min to heat reactor, 30 minutes to cool again
- Limited range of applicable control parameters before boiling or freezing of water
- Unable to determine ultimate gain for sustained oscillations to test tuning methods

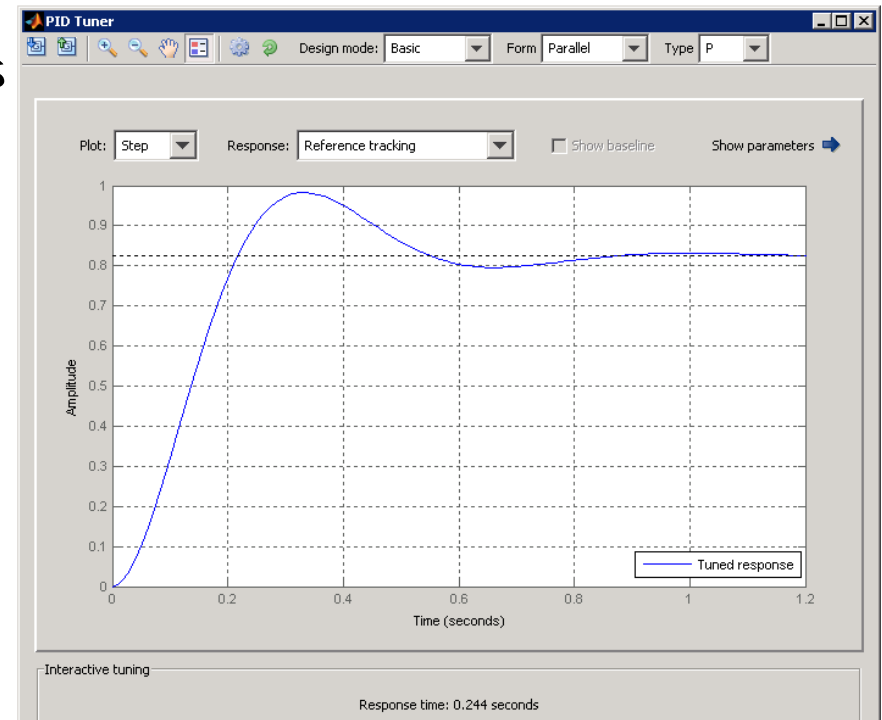
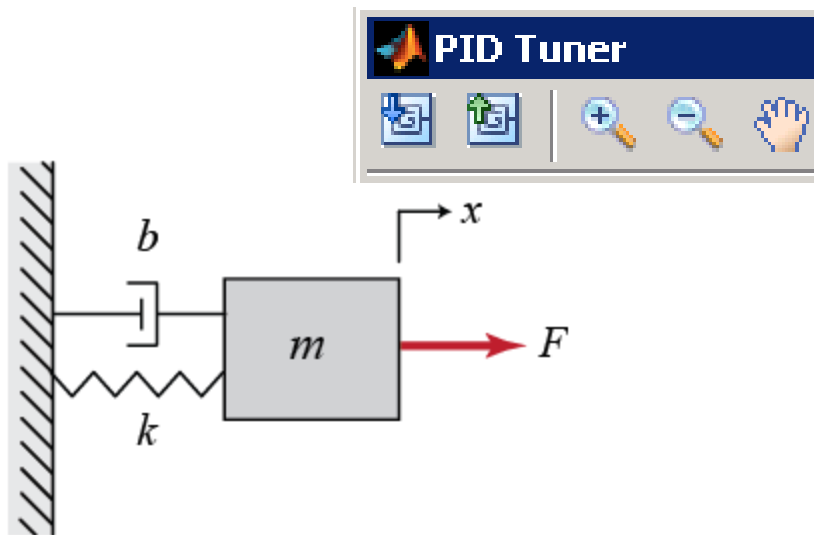
Ziegler-Nichols $K_p = 0.45 K_u$
 $K_i = 1.2 / P_u$



MATLAB PID Tuner Application

MATLAB PID Tuner Application with University of Michigan tutorial:
<http://ctms.engin.umich.edu/CTMS/index.php?example=Introduction§ion=ControlPID#28>

- Good learning tool
- Mass, spring, damper not ChE process
- Transfer function based analysis
- Not “lab experiment”



COMSOL Multiphysics Model of Reactor

Captures essential physics of the process

- 2-D axial symmetry
- Hose outlet connects to inlet via periodic b.c.
- Turbulent flow, k- ϵ model
- Coupled with energy balance
- $Q(t)$ is volume heat source in temperature bath

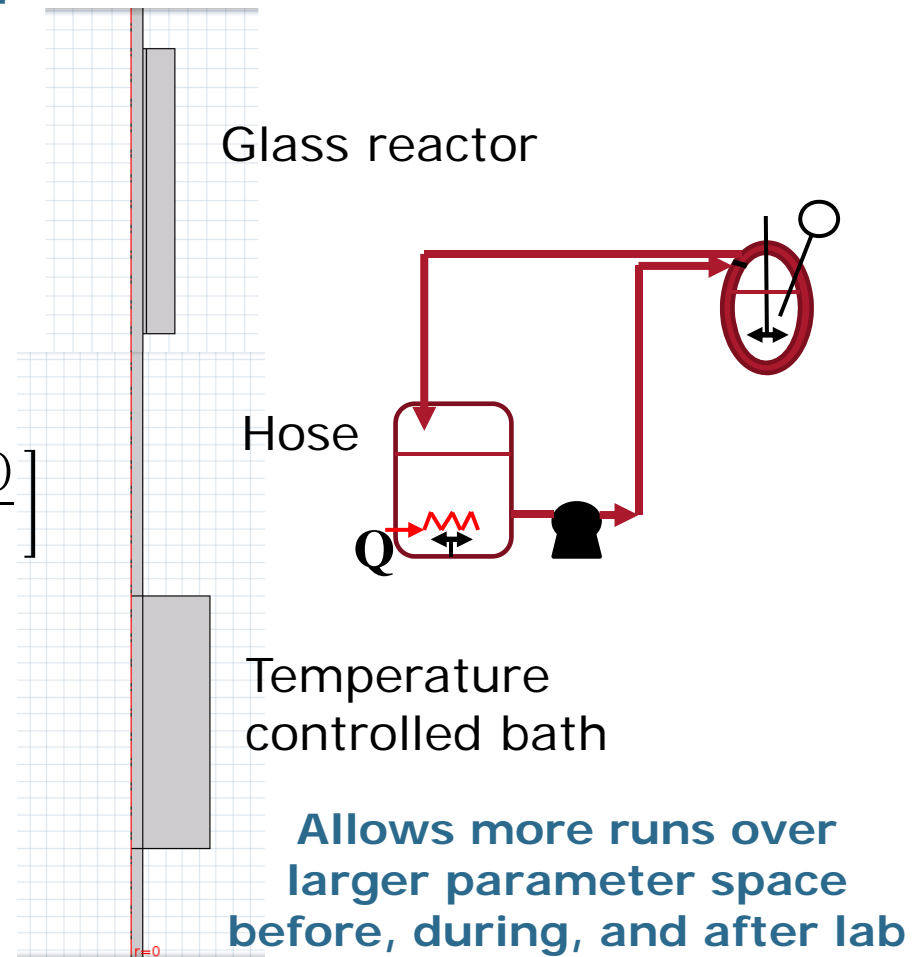
$$Q(t) = Q_o \left[K_P E(t) + K_I \int_0^t E(t) dt + K_D \frac{dE(t)}{dt} \right]$$

Estimated:

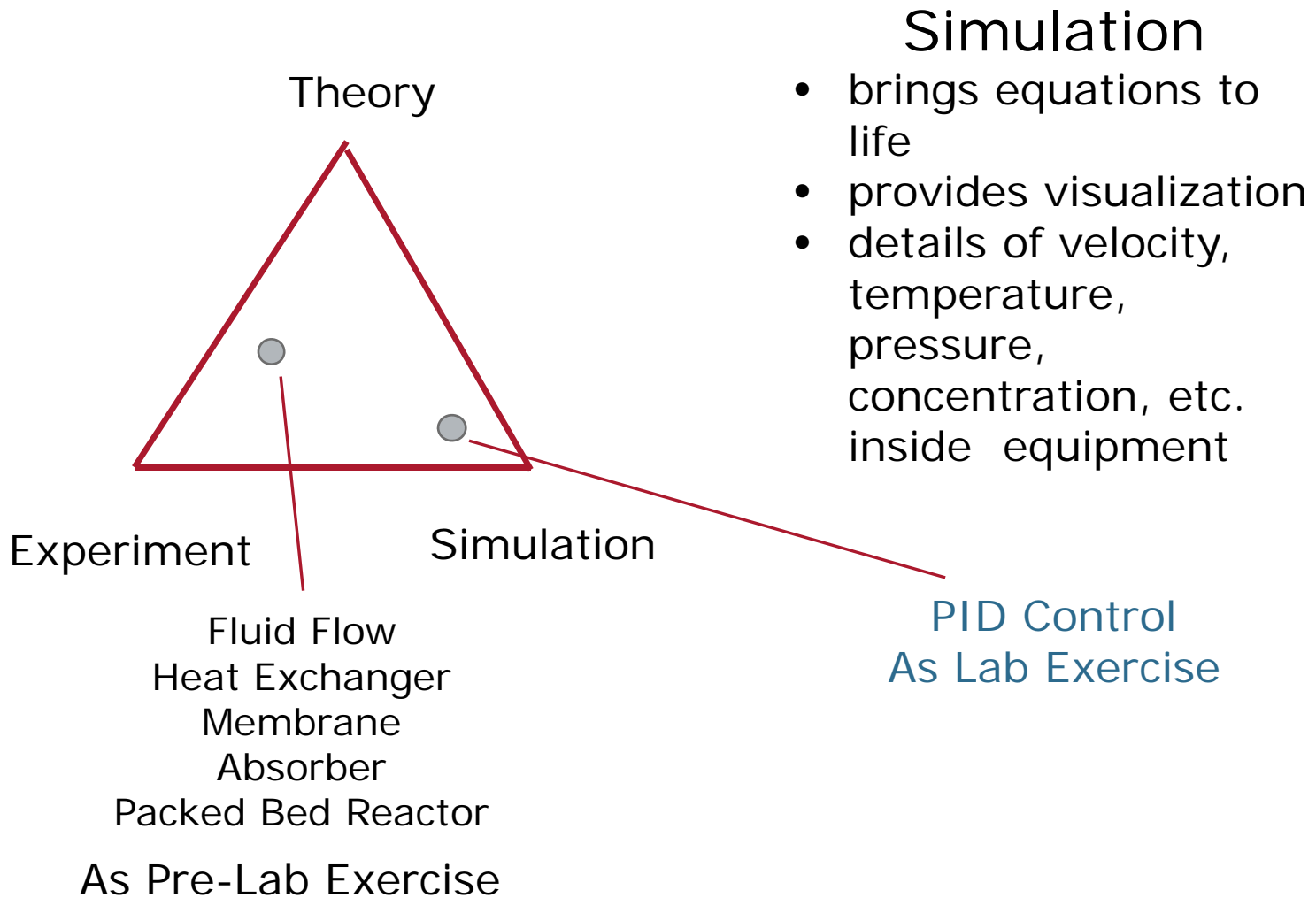
- Flow rate, hose, bath, and jacket volumes
- Heat transfer coefficients
- Heat loss

Assumed:

$$Q_o \text{ cooling} = - Q_o \text{ heating}$$



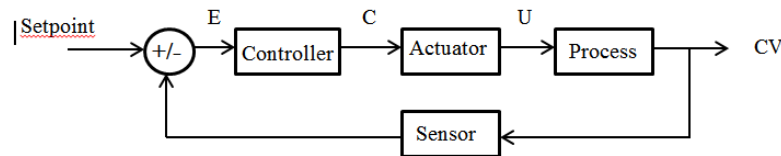
COMSOL Multiphysics in Lab



- brings equations to life
- provides visualization
- details of velocity, temperature, pressure, concentration, etc. inside equipment

Lab Description and Objectives

Brief introduction to practical aspects of process control and PID controller tuning methods



PID control

$$Q(t) = Q_o \left[K_P E(t) + K_I \int_0^t E(t)dt + K_D \frac{dE(t)}{dt} \right]$$

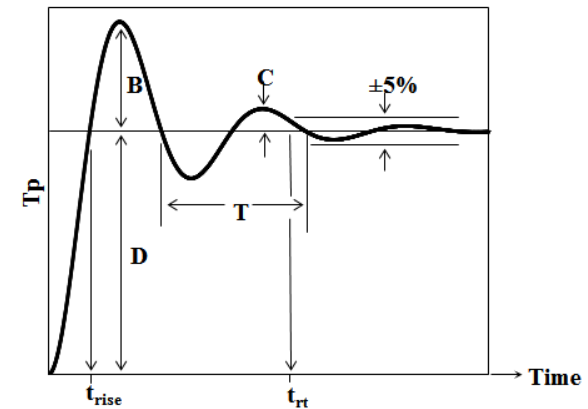


Figure 5. Response for an under damped controlled process [1].

Table 1. Definition of terms in process under damped response.

Term	Definition
Rise time	t_{ris} , the time required for T_p to first reach T_{sp}
Overshoot	B/D
Decay ratio	C/B, ratio of height of successive peaks
Period of oscillation	T, time for a complete cycle
Response time (settling time)	t_{rt} , time required for response to remain within $\pm 5\%$ of T_{sp} , i.e. $T_{sp} \pm 0.05 T_{sp}$.

$$IAE = \int_0^{\infty} |E(t)| dt$$

Lab Description and Objectives

Table 2. Ziegler-Nichols and Tyreus-Luyben PID Controller Settings

Tuning Methods

Controller	Ziegler-Nichols			Tyreus-Luyben		
	K_P	K_I	K_D	K_P	K_I	K_D
P	$0.5 K_U$	-	-	-NA-	-NA-	-NA-
PI	$0.45 K_U$	$1.2/P_U$	-	$0.31 K_U$	$0.45/P_U$	-
PID	$0.6 K_U$	$2/P_U$	$P_U/8$	$0.45 K_U$	$0.45/P_U$	$P_U/6.3$

Riggs method

Objectives:

Before going to lab:

1. Study background material and tutorial on the COMSOL simulation
2. Use simulation to study P-only control. Discover the effect of changing P.

During the lab:

1. Use simulation to find K_U and P_U
2. Use simulation to study Z-N, T-L, and Riggs tuning methods
3. Use simulation to discover effect of K_i and K_d
4. Evaluate IAE for each run and seek to minimize IAE
5. Run at least 3 physical experiments to demonstrate effect of changing parameters K_p and K_i

Lab Description and Objectives

Objectives:

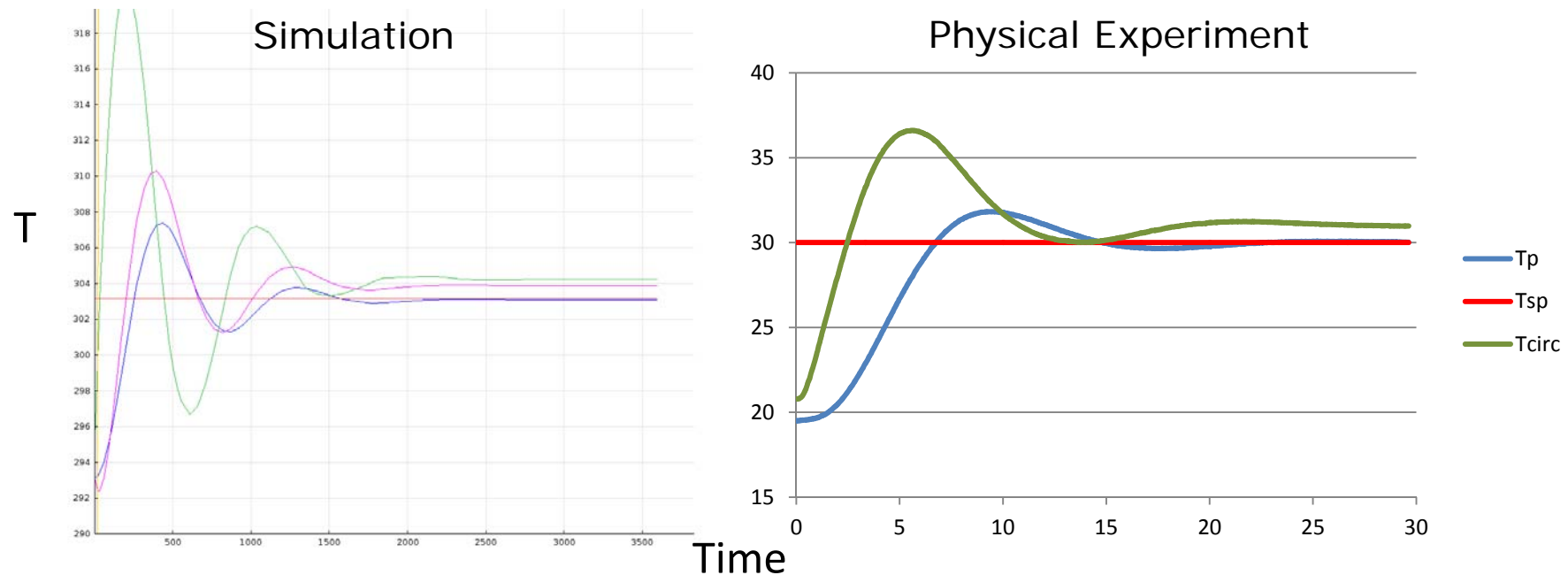
After the lab:

1. Use simulation as needed to understand effect of K_p , K_i , and K_d
2. Find best parameters that give lowest IAE and or “best” control
3. Written report to include:
 - Explanation of the main effect of each parameter,
 - Critique of the three tuning methods studied,
 - Discussion of the physical experiment results,
 - Parameters that gave lowest IAE or “best” control

Contest with promise of a “prize” for group that found the lowest IAE

Many groups already found K_u and P_u and “discovered” or demonstrated the effect of K_i and K_d , as well as K_p , at the pre-lab stage

Results



- Most correctly identified the main effect of K_p , K_i , and K_d , but some failed to see the interdependence
- Some expected Z-N and/or T-L to give optimal results without further refinement
- Some expected the simulation to be perfect
- Many enjoyed the competition to find the lowest IAE

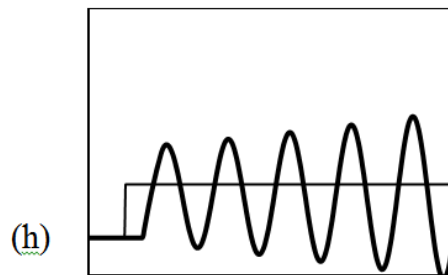
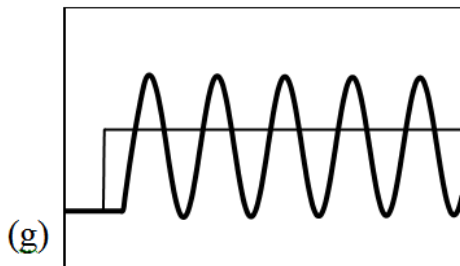
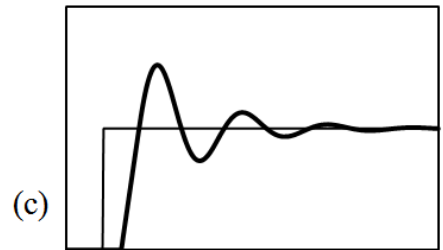
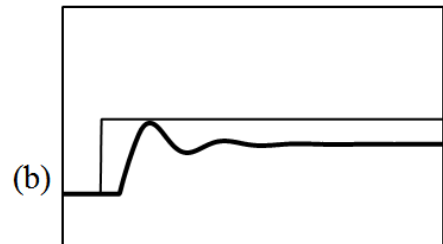
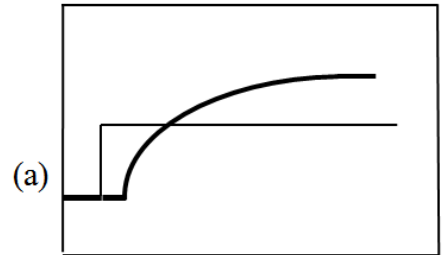
Assessment: Pre / Post Quiz

1. Which figure above looks like a typical open-loop control response curve?

- (a) (b) (f) (h)

3. When using the Ziegler-Nichols tuning method, the closed-loop response curve used for determining the ultimate gain should look like which figure above?

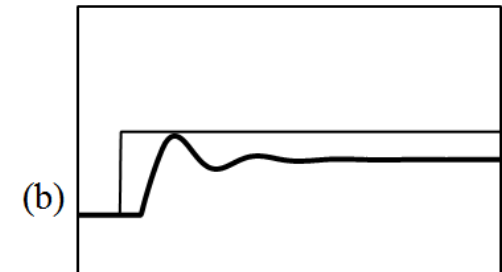
- (c) (e) (g) (h)



Assessment: Pre / Post Quiz

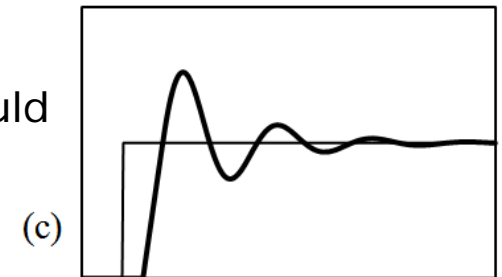
7. Regarding a setpoint change and a PID process controller, the primary benefit of increasing the proportional control parameter is

- (a) increasing the speed of the response
- (b) eliminating offset of the response
- (c) reducing the oscillatory nature of the response
- (d) increasing the setpoint

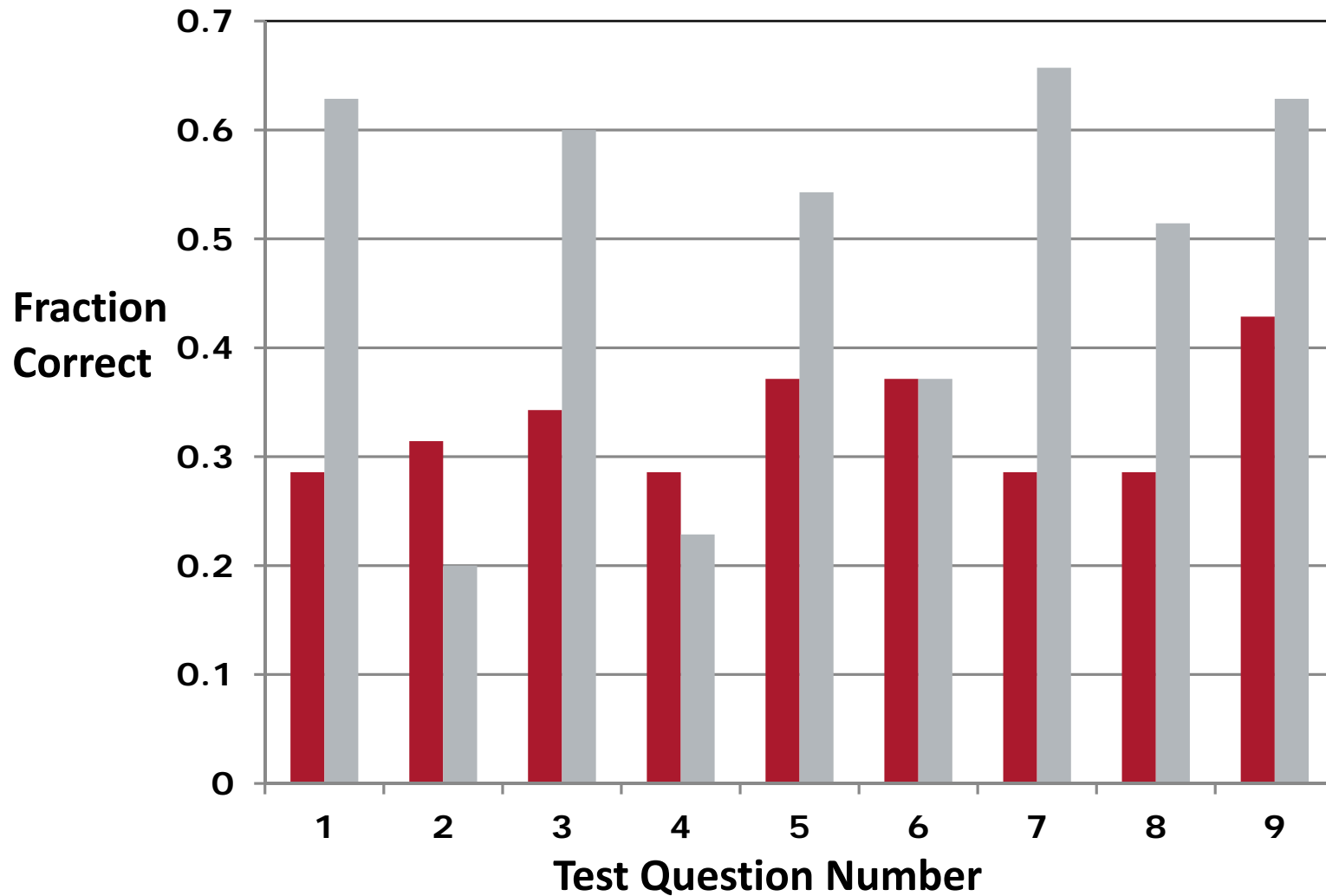


4. When using a PID controller for a set point change, to change the response from figure (b) to figure (c) you should

- (a) increase the proportional control parameter, K_p
- (b) increase the integral control parameter, K_i
- (c) increase the derivative control parameter, K_d
- (d) increase all three parameters



Assessment: Pre / Post Quiz



Assessment: Attitude Survey

Question	a	b	c	d	e
1. If you were to do this again, would you rather run:	only physical experiments	only simulations	one physical experiment and many simulations	3 physical experiments and many simulations	more than 3 experiments and fewer simulations
	3 %	3 %	22 %	53 %	19 %
2. Using the simulation software was:	very difficult	difficult	neither difficult nor easy	easy	very easy
	0 %	0 %	44 %	42 %	14 %
3. Simulation helped me to understand PID control:	not at all	just a little	somewhat	much	very much
	0 %	0 %	28 %	53 %	19 %
4. Simulation helped me to understand PID tuning methods:	not at all	just a little	somewhat	much	very much
	0 %	3 %	44 %	30 %	22 %

Conclusion

- Experiment combined three or four physical experiments with extensive computer simulations,
- Discovered the main effect of proportional, integral, and derivative control parameters,
- Evaluated three parameter tuning methods,
- Obtained “optimal” control by minimizing integral absolute error,
- New experiment was well received by the students,
- Some wanted more physical experiments and to bring the simulation and experiment in closer agreement,
- Interesting, enjoyable, and effective way to teach practical aspects of process control.

Enrollment in our second semester control course went from $< 50\%$ to $> 66\%$ of seniors after this lab was introduced.

ABET visit result not final but preliminary indications are good.