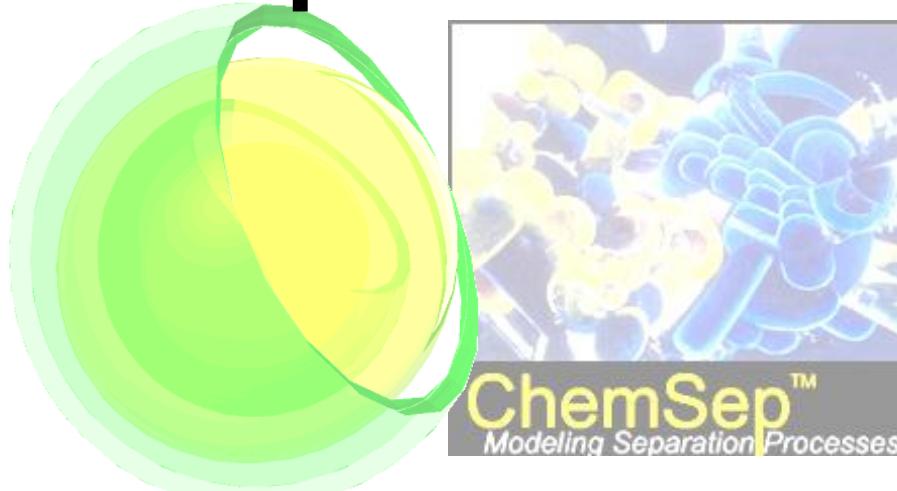


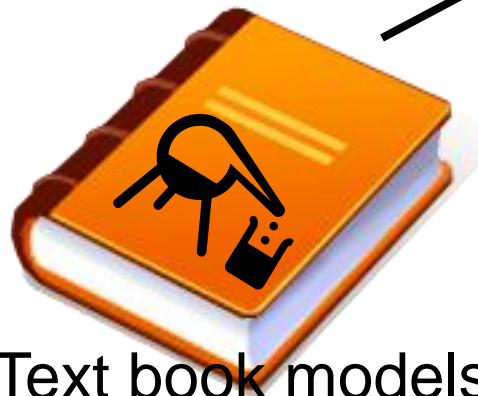
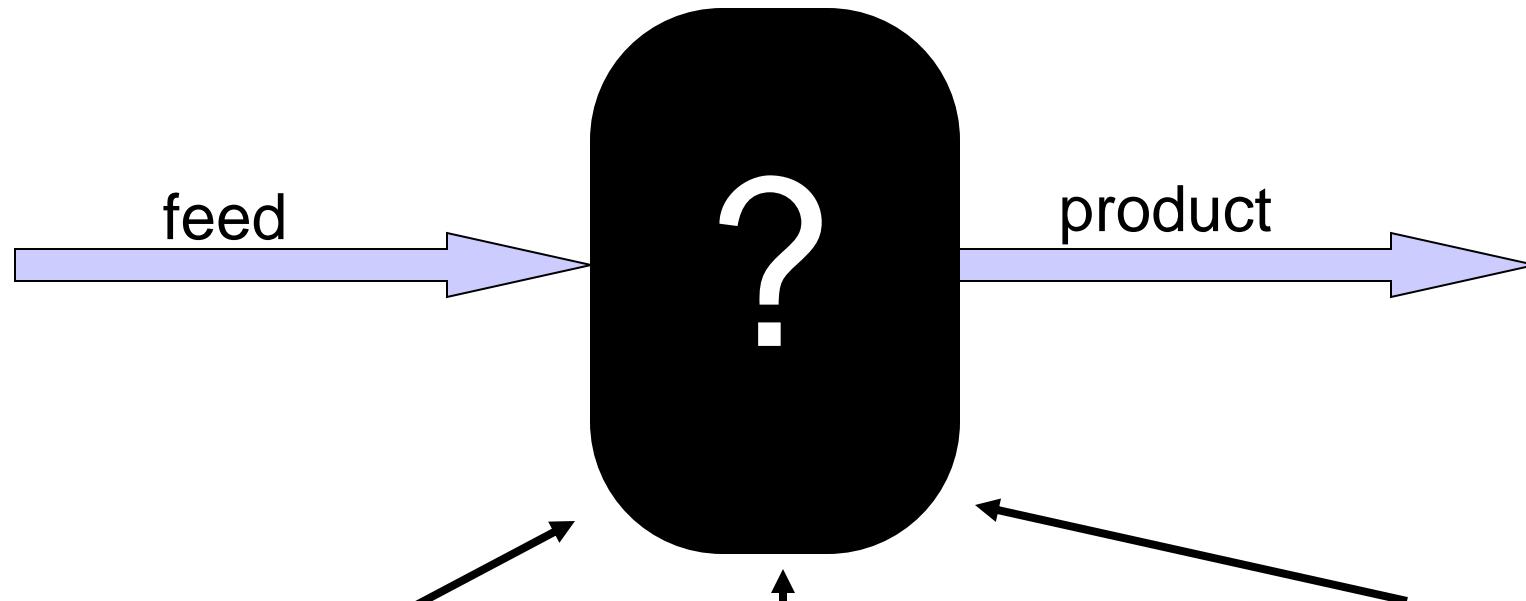
ChemSep, COCO and other modeling tools for versatility in custom process modeling



Jasper van Baten – AmsterCHEM
Ross Taylor – Clarkson University & Chemsep
Harry Kooijman – Clarkson University & Chemsep

Introduction

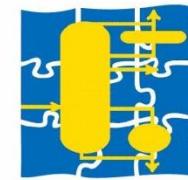
Unit Operation



Text book models

```
SUBROUTINE USERMODEL (NSTREAM, STREAMDATA, ...)  
INTEGER NSTREAM  
DOUBLE PRECISION STREAMDATA(*)  
INCLUDE 'SIMDETAILS.INC'  
SET UP A REFERENCE TO PRESSURE  
STREAMINDEX=PRESSURE_OFFSET_STREAM_1  
|
```

User FORTRAN



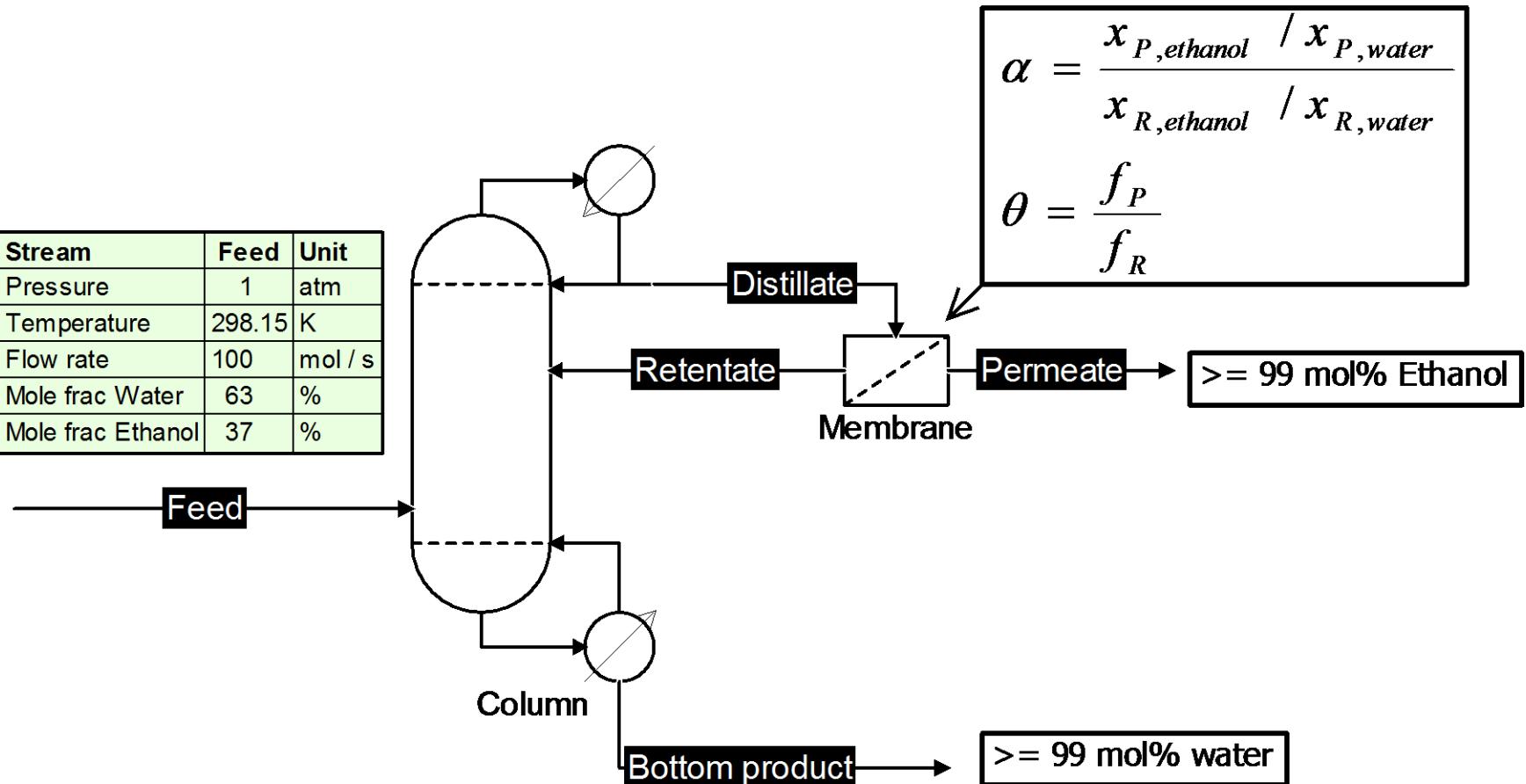
CO_VLaN
CAPE-OPEN

Presentation outline

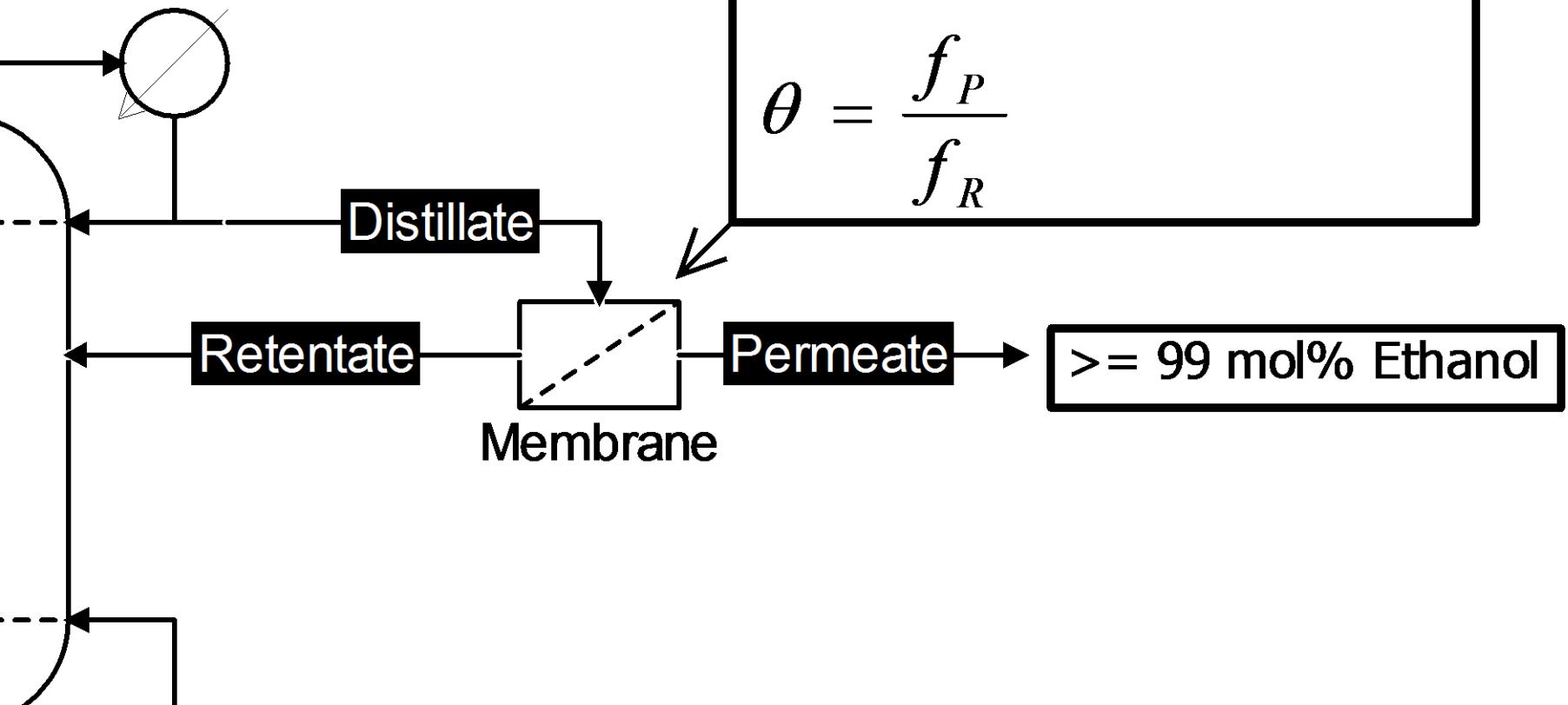
- Introduction
- Example problem specification
- Scilab Unit Operation
- Closing the loop
- Excel Unit Operation
- Conclusions

Example problem specification I

Stream	Feed	Unit
Pressure	1	atm
Temperature	298.15	K
Flow rate	100	mol / s
Mole frac Water	63	%
Mole frac Ethanol	37	%



Example problem specification II



Example problem specification III

 **Property pack definition:**

Package Mode Configure Help

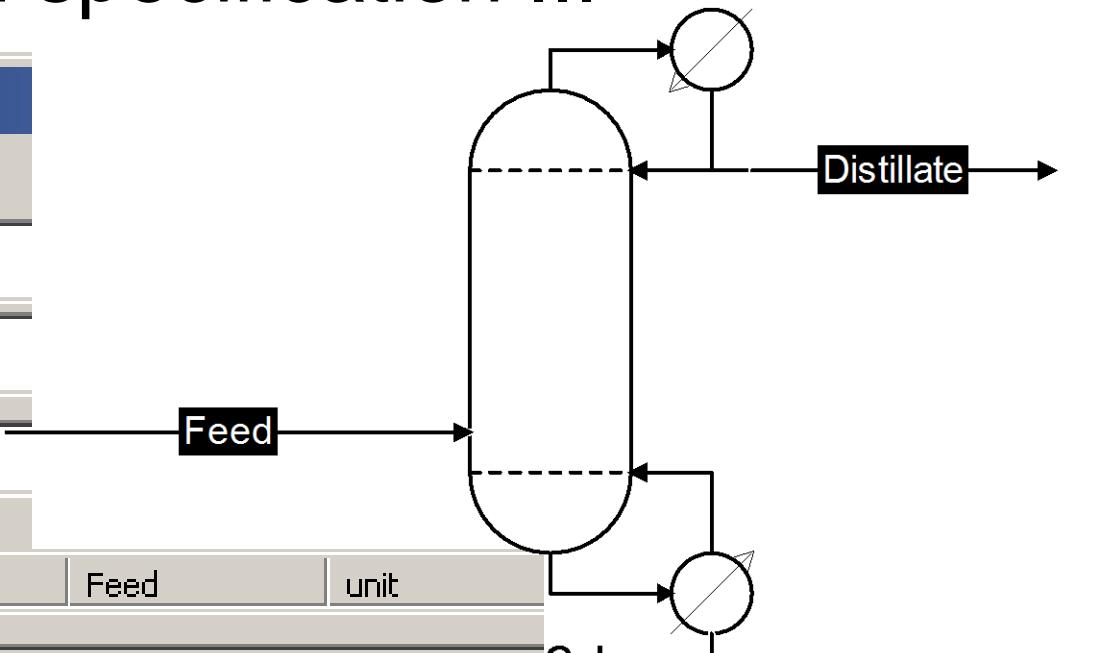
Name: water-ethanol

Description:

Model set: NRTL

Compounds:

Water	Stream	Feed	unit
Water	Stream	1	atm
Ethanol	Connections	298.15	K
	Overall	63	%
	pressure	37	%
	temperature	100	mol / s
	mole fraction [Water]	MW	28.39498 g / mol
	mole fraction [Ethanol]	Compound flows	
	flow	Phase Fractions	
	MW	Liquid composition	



Scilab Unit operation I

 **SciLab CAPE-OPEN Unit Operation:**

Ports Parameters Reports SciLab Additional files About

Feed ports:

Name	#	Connected to
Feed	1	

Product ports:

Name	#	Connected
Permeate	1	
Retentate	2	

Scilab Unit operation II

SciLab CAPE-OPEN Unit Operation:

Name	Type	Direction	Value	Default	Min	Max	Unit of measure
sepFactor	Real	Input	70				
cut	Real	Input	0.6				

Scilab Unit operation III

// compound indices:

```
water=1;  
ethanol=2;
```

//parameter values:

```
alpha=getParameter('sepFactor');  
theta=getParameter('cut');
```

//feed values

```
XF=getFeedProp(1,'fraction');  
FF=getFeedProp(1,'totalFlow');  
TF=getFeedProp(1,'temperature');  
PF=getFeedProp(1,'pressure');
```

//product flows (explicit solution of theta=FP/FR and FF=FP+FR):

```
FR=FF/(theta+1);  
FP=theta*FR;
```

Scilab Unit operation IV

//function to calculate compositions from XPE:

```
function [XP,XR]=GetCompositions(XPE)
XP=[1-XPE,XPE];
XRE=(FF*XF(ethanol)-FP*XPE)/FR;
XR=[1-XRE,XRE];
endfunction
```

//function to solve compositions

```
function errorValue=CompositionFunction(XPE)
```

//get the compositions given XPE:

```
[XP,XR]=GetCompositions(XPE);
```

//return the error in alpha

```
errorValue= (XP(ethanol)/XP(water))/(XR(ethanol)/XR(water))-alpha;
```

```
endfunction
```

Scilab Unit operation VI

//solve for the compositions to match alpha:

```
XPE=fsolve(0.999,CompositionFunction);
```

//the compositions at solutions are then

```
[XP,XR]=GetCompositions(XPE);
```

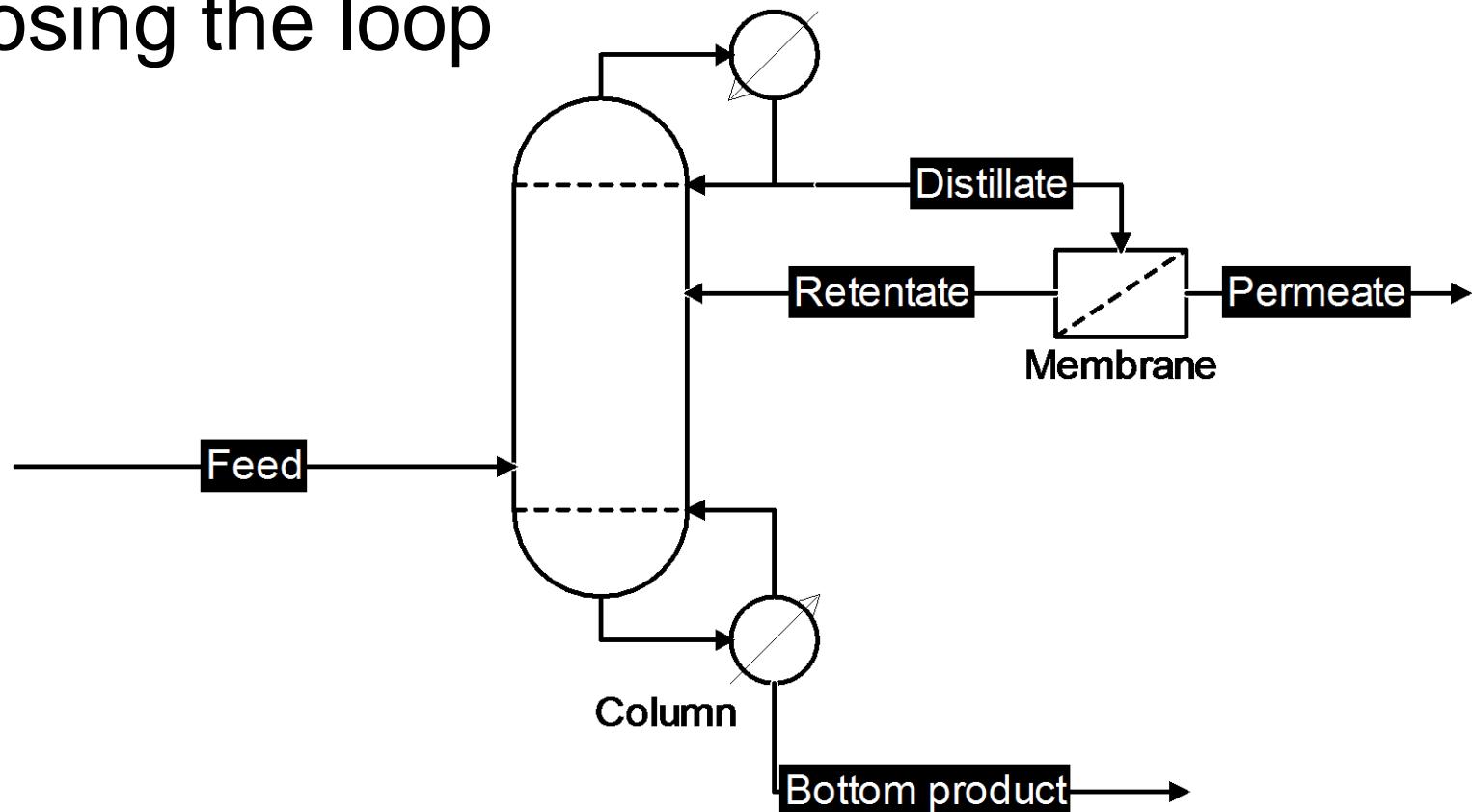
//set the permeate, given FP, XP, TF, PF

```
setProduct(1,FP,XP,'temperature',TF,'pressure',PF);
```

//set the retentate, given FR, XR, TF, PF

```
setProduct(2,FR,XR,'temperature',TF,'pressure',PF);
```

Closing the loop



Stream	Feed	Distillate	Retentate	Permeate	Bottom product	Unit
Pressure	1	1	1	1	1	atm
Temperature	298.15	351.471	351.471	351.471	373.774	K
Flow rate	100	98.9368	61.8355	37.1013	62.9987	mol / s
Mole frac Water	63	15	23.7344	0.442615	99.9	%
Mole frac Ethanol	37	85	76.2655	99.5574	0.1	%

Excel Unit Operation I

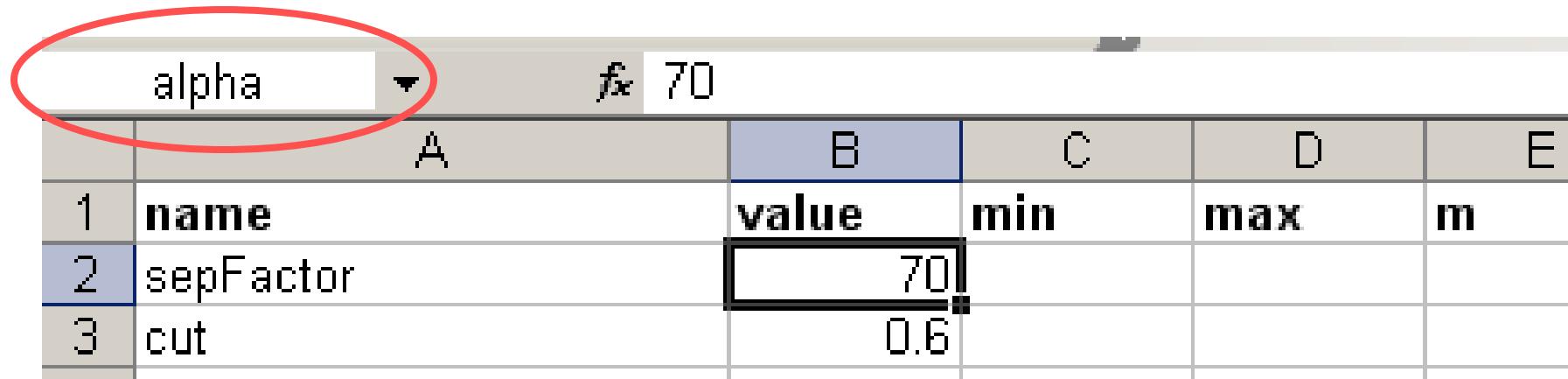
	A	B	C	D	E	F	G	H	I
1		T	P	H	flow	mole fractions			
2	Name	[K]	[Pa]	[J/mol]	[mol/s]				
3	Feed								
4									
5									
6									
7									
8									
9									
10									

control \ feeds \ products \ input parameters \ output parameters \ calculations /

Excel Unit Operation II

	A	B	C	D	E	F	G	H
1		T	P	H	flow	mole fractions		
2	Name	[K]	[Pa]	[J/mol]	[mol/s]			
3	Permeate							
4	Retentate							

Excel Unit Operation III



	A	B	C	D	E
1	name	value	min	max	m
2	sepFactor	70			
3	cut	0.6			
.					

Excel Unit Operation V

	A	B	C	
1	F retentate	=feeds!E3/(theta+1)	mol/s	
2	F permeate	=theta*B1	mol/s	
3				
4	X p ethanol guess	0.999	mol/mol	Initial guess f
5	X p ethanol	0.999	mol/mol	Will be solved
6	X p water	=1-B5	mol/mol	
7	X r ethanol	=((feeds!E3*feeds!G3-B2*B5)/B1	mol/mol	
8	X r water	=1-B7	mol/mol	
9				
10	alpha	=(B5/B6)/(B7/B8)		
11	error	=B10-alpha		
12				

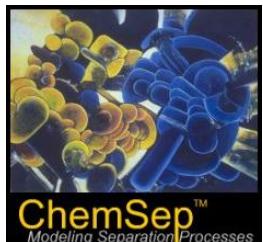
Excel Unit Operation VI

	A	B	C	D	E	F
1		T	P	H	flow	mole fractions
2	Name	[K]	[Pa]	[J/mol]	[mol/s]	Water
3	Permeate	=feeds!B3	=feeds!C3		=calculations!B2	=calculations!B6
4	Retentate	=feeds!B3	=feeds!C3		=calculations!B1	=calculations!B8
5						

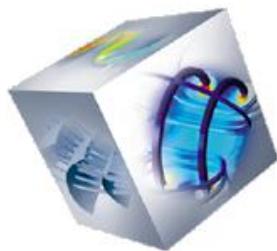
Conclusions:

- Need for custom models
- Only enter model equations
- Use existing solvers
- Solutions: Scilab, Matlab, Excel
- Context: CAPE-OPEN
- Simulation environment: COCO / ChemSep
- Suitable for research and teaching

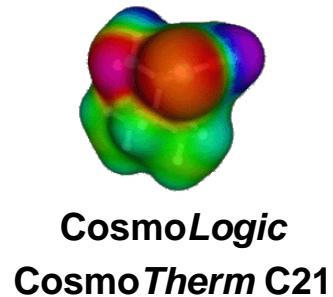
- Download COCO: <http://www.cocosimulator.org/>
- ChemSep: <http://www.chemsep.com/>
- CAPE-OPEN standards: <http://www.colan.org/>
- Matlab, Scilab, Excel Unit Operations:
<http://www.amsterchem.com/>



ChemSep™
Modeling Separation Processes



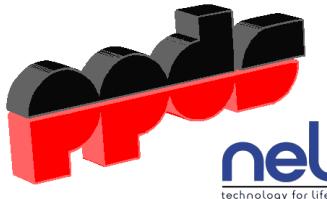
COMSOL
Multiphysics 4.2



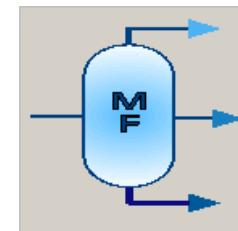
CosmoLogic
CosmoTherm C21



EPA WAR &
.NET libraries



TUV-NEL
PPDS v4.1.0.0



Infochem
Multiflash 3.9

